

# MECHANICS OF FLUIDS

Lecture 8 – Energy Equation  
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# Note

- All the art-work contents of this lecture are obtained from the following sources, unless otherwise stated:
  - *Fluid Mechanics, 8<sup>th</sup> edition, Frank M. White, McGraw-Hill, 2016.*
  - *Fluid Mechanics: Fundamental and Applications, 3<sup>rd</sup> edition, Yunus A. Cengel, John M. Cimbala, McGraw-Hill, 2014.*

# System analysis

- The **first law of thermodynamics** for a closed system
  - *The energy change of the system during a process is equal to the received heat added to system minus the work done by system.*

$$\frac{dQ}{dt} - \frac{dW}{dt} = \frac{dE}{dt}$$

- Using Reynolds transport theorem, this can be expressed for a control volume:

$$\frac{d}{dt} (B_{\text{syst}}) = \frac{d}{dt} \left( \int_{\text{CV}} \beta \rho d\mathcal{V} \right) + \int_{\text{CS}} \beta \rho (\mathbf{V}_r \cdot \mathbf{n}) dA$$

$\downarrow$   $E$ 
 $\swarrow$ 
 $\searrow$

$e = dE/dm$

# System analysis

$$\frac{dQ}{dt} - \frac{dW}{dt} = \frac{dE}{dt} = \frac{d}{dt} \left( \int_{CV} e \rho d\mathcal{V} \right) + \int_{CS} e \rho (\mathbf{V} \cdot \mathbf{n}) dA \quad (*)$$

Rate of heat added to system (through CS)

Rate of work done by system

$$e = e_{\text{internal}} + e_{\text{kinetic}} + e_{\text{potential}}$$

$$e = \hat{u} + \frac{1}{2}V^2 + gz$$

We leave this to Heat Transfer course

$$\dot{W}_{\text{shaft}} + \dot{W}_{\text{press}} + \dot{W}_{\text{viscous stresses}} = \dot{W}_s + \dot{W}_p + \dot{W}_v$$

# System analysis

- $\dot{W}_s$  is energy rate out of control volume through **shaft work**, like pump, turbine, fan and etc.

- **Pressure work:**

$$d\dot{W}_p = -(p \, dA) V_{n, \text{in}} = -p(-\mathbf{V} \cdot \mathbf{n}) \, dA$$

$$\dot{W}_p = \int_{\text{CS}} p(\mathbf{V} \cdot \mathbf{n}) \, dA$$

- And similarly the **shear work** is:

$$\dot{W}_v = - \int_{\text{CS}} \boldsymbol{\tau} \cdot \mathbf{V} \, dA$$

# System analysis

- Substitution into the main equation (\*), we get:

$$\dot{Q} - \dot{W}_s - \dot{W}_v = \frac{\partial}{\partial t} \left( \int_{CV} e \rho d\mathcal{V} \right) + \int_{CS} \left( e + \frac{p}{\rho} \right) \rho (\mathbf{V} \cdot \mathbf{n}) dA$$

$$e = \hat{u} + \frac{1}{2}V^2 + gz \quad \downarrow \quad \hat{h} = \hat{u} + p/\rho$$

$$\dot{Q} - \dot{W}_s - \dot{W}_v = \frac{\partial}{\partial t} \left[ \int_{CV} \left( \hat{u} + \frac{1}{2}V^2 + gz \right) \rho d\mathcal{V} \right] + \int_{CS} \left( \hat{h} + \frac{1}{2}V^2 + gz \right) \rho (\mathbf{V} \cdot \mathbf{n}) dA$$

# Energy equation of steady flow

- For a control volume at **steady condition** with **one inlet** and **one outlet** and **uniform flow** at inlet and outlet:

$$\dot{Q} - \dot{W}_s - \dot{W}_v = -\dot{m}_1(\hat{h}_1 + \frac{1}{2}V_1^2 + gz_1) + \dot{m}_2(\hat{h}_2 + \frac{1}{2}V_2^2 + gz_2)$$

- And considering the fact that  $\dot{m}_1 = \dot{m}_2 = \dot{m}$

$$\underbrace{\hat{h}_1 + \frac{1}{2}V_1^2 + gz_1}_{\text{Stagnation enthalpy at inlet}} = \underbrace{(\hat{h}_2 + \frac{1}{2}V_2^2 + gz_2)}_{\text{Stagnation enthalpy at outlet}} - q + w_s + w_v$$

Stagnation enthalpy  
at inlet

Stagnation enthalpy  
at outlet

$$q = \dot{Q}/\dot{m}$$

$$w_s = \dot{W}_s/\dot{m}$$

$$w_v = \dot{W}_v/\dot{m}$$

What does this equation mean?

# Energy equation of steady flow

- If we divide this equation by  $g$ , the dimension of each term becomes **length** [m or ft]:

$$\frac{p_1}{\gamma} + \frac{\hat{u}_1}{g} + \frac{V_1^2}{2g} + z_1 = \frac{p_2}{\gamma} + \frac{\hat{u}_2}{g} + \frac{V_2^2}{2g} + z_2 - h_q + h_s + h_v$$



# For a pipe system with incompressible flow

- Assuming no heat transfer with surroundings ( $h_q=0$ ).
- The friction losses exist in the control volume, they irreversibly convert the mechanical energy to internal energy.


$$\frac{\hat{u}_2 - \hat{u}_1}{g} = h_{friction}$$

- Assuming negligible viscous work at inlet and outlet ( $h_v = 0$ ).
- The shaft work can be either pump work on fluid (negative in our convention) or turbine work (positive in our convention)

$$h_s = -h_{pump} + h_{turbine}$$

# For a pipe system with incompressible flow

$$\underbrace{\left(\frac{p}{\gamma} + \frac{V^2}{2g} + z\right)}_{\text{Total head at inlet}}_{\text{in}} = \underbrace{\left(\frac{p}{\gamma} + \frac{V^2}{2g} + z\right)}_{\text{Total head at outlet}}_{\text{out}} + h_{\text{friction}} - h_{\text{pump}} + h_{\text{turbine}}$$



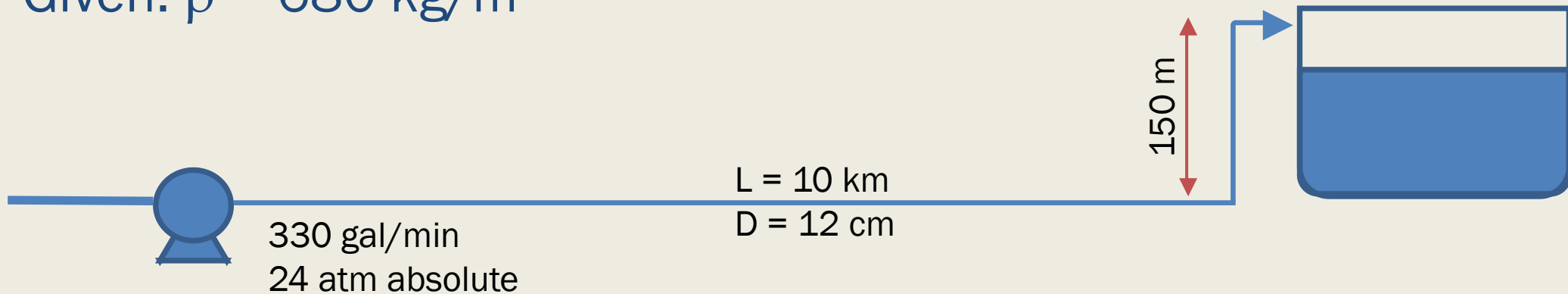
Friction/head loss      Head added by pump      Head produced by turbine

# Example 1

Gasoline at 20 °C is pumped through a smooth 12-cm-diameter pipe 10 km long, at a flow rate of 75 m<sup>3</sup>/h (330 gal/min). The inlet is fed by a pump at an absolute pressure of 24 atm. The exit is at standard atmospheric pressure and is 150 m higher. Estimate the frictional head loss  $h_f$ , and compare it to the velocity head of the flow.

Answer:  $h_f = 199$  m

Given:  $\rho = 680$  kg/m<sup>3</sup>



# Example 1

- Energy equation with  $h_{pump} = h_{turbine} = 0$

$$\frac{p_{in}}{\gamma} + \frac{V_{in}^2}{2g} + z_{in} = \frac{p_{out}}{\gamma} + \frac{V_{out}^2}{2g} + z_{out} + h_f$$

- Average inlet and outlet velocities:

$$V_{in} = V_{out} = \frac{Q}{A} = \frac{Q}{(\pi/4)D^2} = \frac{(75 \text{ m}^3/\text{h})/(3600 \text{ s/h})}{(\pi/4)(0.12 \text{ m})^2} \approx 1.84 \frac{\text{m}}{\text{s}}$$

$$\frac{(24)(101,350 \text{ N/m}^2)}{6670 \text{ N/m}^3} + 0.173 \text{ m} + 0 \text{ m} = \frac{101,350 \text{ N/m}^2}{6670 \text{ N/m}^3} + 0.173 \text{ m} + 150 \text{ m} + h_f$$

$$h_f = 364.7 - 15.2 - 150 \approx 199 \text{ m}$$

# Kinetic energy correction factor

- Recall that in energy equation (steady condition) there is a term containing fluid velocity:

$$\dot{Q} - \dot{W}_s - \dot{W}_v = \int_{CS} \left( \hat{h} + \frac{1}{2}V^2 + gz \right) \rho(\mathbf{V} \cdot \mathbf{n}) dA$$

- We obtained the following equation by **assuming an average uniform flow** at inlet and outlet:

$$\dot{Q} - \dot{W}_s - \dot{W}_v = -\dot{m}_1 \left( \hat{h}_1 + \frac{1}{2}V_1^2 + gz_1 \right) + \dot{m}_2 \left( \hat{h}_2 + \frac{1}{2}V_2^2 + gz_2 \right)$$

# Kinetic energy correction factor

- This assumption can be erroneous and should be modified by inserting a correction factor into the energy equation as follows:

$$\dot{Q} - \dot{W}_s - \dot{W}_v = -\dot{m}_1(\hat{h}_1 + \alpha \frac{1}{2} V_1^2 + gz_1) + \dot{m}_2(\hat{h}_2 + \alpha \frac{1}{2} V_2^2 + gz_2)$$

$$\int_{\text{port}} (\frac{1}{2} V^2) \rho (\mathbf{V} \cdot \mathbf{n}) dA \equiv \alpha (\frac{1}{2} V_{\text{av}}^2) \dot{m} \quad V_{\text{av}} = \frac{1}{A} \int u dA$$

- If  $u$  is the velocity normal to the surface:

$$\frac{1}{2} \rho \int u^3 dA = \frac{1}{2} \rho \alpha V_{\text{av}}^3 A \quad \Rightarrow \quad \alpha = \frac{1}{A} \int \left( \frac{u}{V_{\text{av}}} \right)^3 dA$$

# Kinetic energy correction factor

- For laminar flow:

$$u = U_0 \left[ 1 - \left( \frac{r}{R} \right)^2 \right]$$

$$V_{\text{av}} = 0.5U_0 \quad \longrightarrow \quad \alpha = 2.0$$

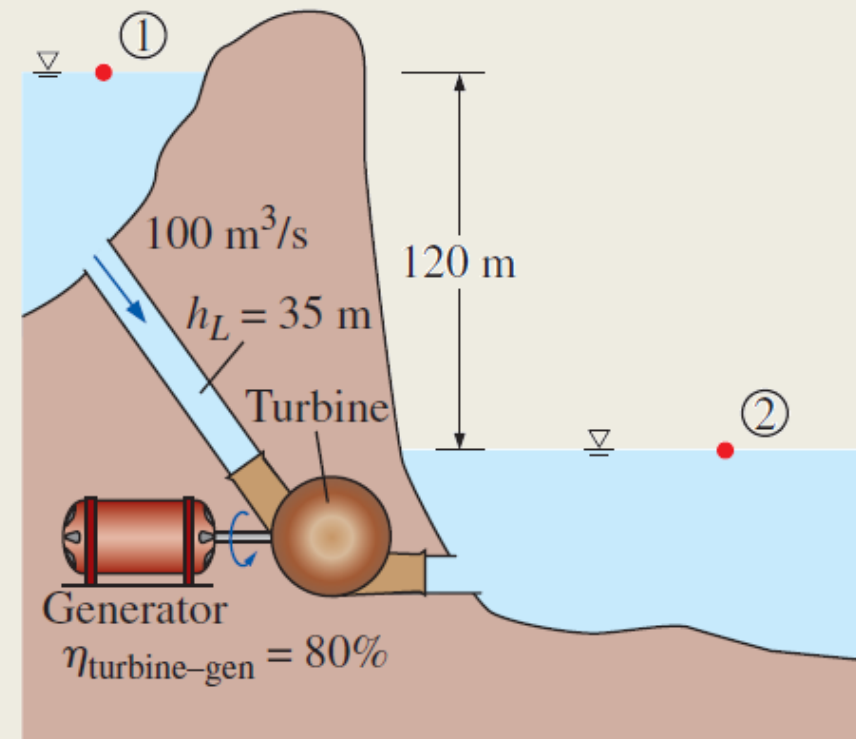
- For turbulent flow:

$$u \approx U_0 \left( 1 - \frac{r}{R} \right)^m \quad \longrightarrow \quad \alpha = \frac{(1+m)^3(2+m)^3}{4(1+3m)(2+3m)}$$

$m$	$\frac{1}{5}$	$\frac{1}{6}$	$\frac{1}{7}$	$\frac{1}{8}$	$\frac{1}{9}$
$\alpha$	1.106	1.077	1.058	1.046	1.037

## Example 2

In a hydroelectric power plant,  $100 \text{ m}^3/\text{s}$  of water flows from an elevation of  $120 \text{ m}$  to a turbine, where electric power is generated. The total irreversible head loss in the piping system from point 1 to point 2 is  $35 \text{ m}$ . If the overall efficiency of the turbine-generator is  $80\%$ , estimate the electric power output.



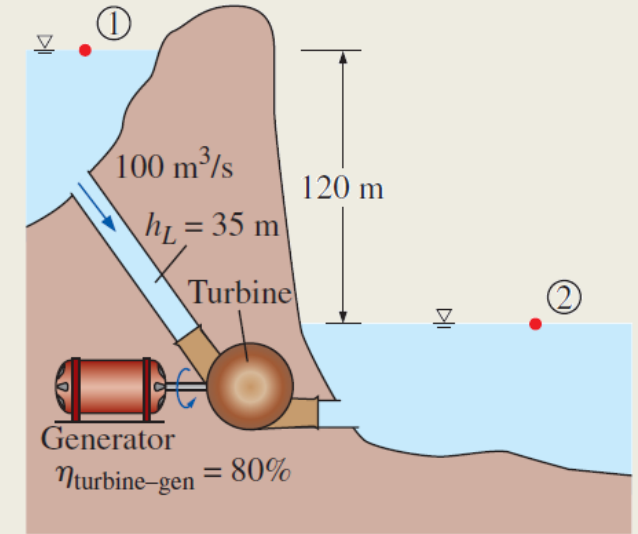


# Example 2

- Energy equation between points 1 and 2:
  - Velocities are negligible.
  - $P_1$  and  $P_2$  are cancelled out.

$$\cancel{\frac{P_1}{\rho g}} + \alpha_1 \cancel{\frac{V_1^2}{2g}} + z_1 + \cancel{h_{\text{pump},u}} = \cancel{\frac{P_2}{\rho g}} + \alpha_2 \cancel{\frac{V_2^2}{2g}} + \cancel{z_2} + h_{\text{turbine},e} + h_L$$

$$\longrightarrow h_{\text{turbine},e} = z_1 - h_L = 120 - 35 = 85 \text{ m}$$



## Example 2

- The mechanical work of turbine:

$$\dot{W}_{\text{turbine}, e} = \dot{m}gh_{\text{turbine}, e} = (10^5 \text{ kg/s})(9.81 \text{ m/s}^2)(85 \text{ m}) \left( \frac{1 \text{ kJ/kg}}{1000 \text{ m}^2/\text{s}^2} \right) = 83,400 \text{ kW}$$

- The electrical output of generator

$$\dot{W}_{\text{electric}} = \eta_{\text{turbine-gen}} \dot{W}_{\text{turbine}, e} = (0.80)(83.4 \text{ MW}) = \mathbf{66.7 \text{ MW}}$$